

Amendments to the Claims:

1. (Currently Amended) ~~Process~~ A process for the treatment of ~~baths~~ a bath for the exhaustion dyeing of cellulose fibres with reactive dyes comprising the steps of prefiltrating the bath to form a prefiltrated bath, neutralizing the prefiltrated bath to form a neutralized bath, nanofiltrating the neutralized bath to form a nanofiltrated bath and performing reverse osmosis on the nanofiltrated bath ~~a prefiltration, then a neutralization, then a nanofiltration and then a reverse osmosis.~~
2. (Currently Amended) ~~Process~~ The process according to Claim 1, which is characterized in that ~~the dye baths are~~ wherein the bath is an industrial bath ~~comprising and in that they comprise hydrolysed reactive dyes which preferably belong to the trichloropyrimidine, difluoropyrimidine, difluoromono-chloropyrimidine, mono-chlorotriazine and vinyl sulphone families.~~
3. (Currently Amended) ~~Process~~ The process according to Claim 1 or 2, which is characterized in that wherein the prefiltration step is carried out with a filter with a membrane having a ~~preferred~~ cutoff threshold of between 80 and 120 microns.
4. (Currently Amended) ~~Process~~ The process according to Claims 1 to 3, which is characterized in that claim 1, wherein the neutralization step is carried out with acid, ~~preferably hydrochloric acid,~~ in the presence or absence of bubbling of air.
5. (Currently Amended) ~~Process~~ The process according to Claims 1 to 4, which is characterized in that, ~~during~~ claim 2, wherein the nanofiltration step further comprises separation with a nanofiltration membrane and wherein the separation, the separation is carried out in an aqueous solution, ~~on the one hand, of and separates~~ inorganic salts present at high concentrations, ~~on the other hand, of from~~

the hydrolysed reactive dyes having masses close to those of the cutoff threshold of the membrane.

6. (Currently Amended) Process according to Claim 5 ~~which is characterized in that feed liquor is continuously introduced wherein the nanofiltration step further comprises continuously introducing the feed liquor~~ into a filtration module comprising a the nanofiltration membrane under a positive pressure to provide a permeate liquor which has passed through the nanofiltration membrane (permeate) and a retentate liquor which has transited without passingnot passed through the nanofiltration membrane (retentate), and wherein the retentate being liquor is continuously directed to ~~the~~ a feed tank.

7. (Currently Amended) ~~Process~~ The process according to Claim 5, ~~which is characterized in that, wherein~~ during the nanofiltration step, hydrolysed reactive dyes are concentrated upstream of the nanofiltration membrane and inorganic salts are removed through the nanofiltration membrane via a concentration step.

8. (Currently Amended) ~~Process~~ The process according to Claim 5, ~~which is characterized in that, wherein~~ during the nanofiltration step, the concentration of hydrolysed reactive dyes upstream of the nanofiltration membrane is kept constant by addition of pure water and the inorganic salts are removed through the nanofiltration membrane via a diafiltration step.

9. (Currently Amended) ~~Process~~ The process according to Claim 5, ~~which is characterized in that the nanofiltration stage can operate wherein the nanofiltration step further comprises removing the inorganic salts and wherein removal of the inorganic salts is accomplished by concentration, or diafiltration followed by concentration or concentration followed by diafiltration followed by concentration.~~
(i) in a single step (concentration),
(ii) in two steps (diafiltration-concentration), or

~~(iii) in three steps (concentration-diafiltration-concentration),
preferably in three steps.~~

10. (Currently Amended) ~~Process~~ The process according to Claim 5, ~~which is characterized in that~~ wherein the initial concentration of inorganic salts is between 30 and 100 g/l.

11. (Currently Amended) ~~Process~~ The process according to ~~Claims 1 to 10,~~ claim 1, ~~which is characterized in that,~~ wherein in the reverse osmosis step, the feed liquor has an initial concentration of inorganic salts of between 5 and 70 g/l, ~~preferably between 10 and 15 g/l.~~

12. (Currently Amended) ~~Process~~ The process according to ~~Claims 1 to 10,~~ claim 1, ~~which is characterized in that the retentate from~~ wherein the reverse osmosis step forms a reverse osmosis retentate, and wherein the reverse osmosis retentate is composed of pure water comprising inorganic salts concentrated to between 3 and 8% by weight, without coloured waste products, at a pH preferably of between 5.5 and 6, ~~and in that it can be reused in dyeing.~~

13. (New) The process according to claim 2, wherein the reactive dyes are selected from the group consisting of which preferably belong to the trichloropyrimidine, difluoropyrimidine, difluoromonochloropyrimidine, monochlorotriazine and vinyl sulphone.

14. (New) The process according to claim 4, wherein the acid is hydrochloric acid.

15. (New) The process according to claim 7, wherein removal of the inorganic salts from the nanofiltration membrane is accomplished by concentration.

16. (New) The process according to claim 8, wherein removal of the inorganic salts from the nanofiltration membrane is accomplished by diafiltration.
17. (New) The process according to claim 1, wherein in the reverse osmosis step, the feed liquor has an initial concentration of inorganic salts of between 10 and 15 g/l.
18. (New) The process according to claim 9, wherein removal is accomplished by concentration or concentration followed by diafiltration followed by concentration.
19. (New) The process according to claim 12, wherein the reverse osmosis retentate can be used in dyeing.
20. (New) A process for exhaustion dyeing cellulose fibers comprising the step of employing the process for the treatment of a bath for exhaustion dyeing according to claim 1.
21. (New) Cellulose fibers made in accordance with the process of claim 20.